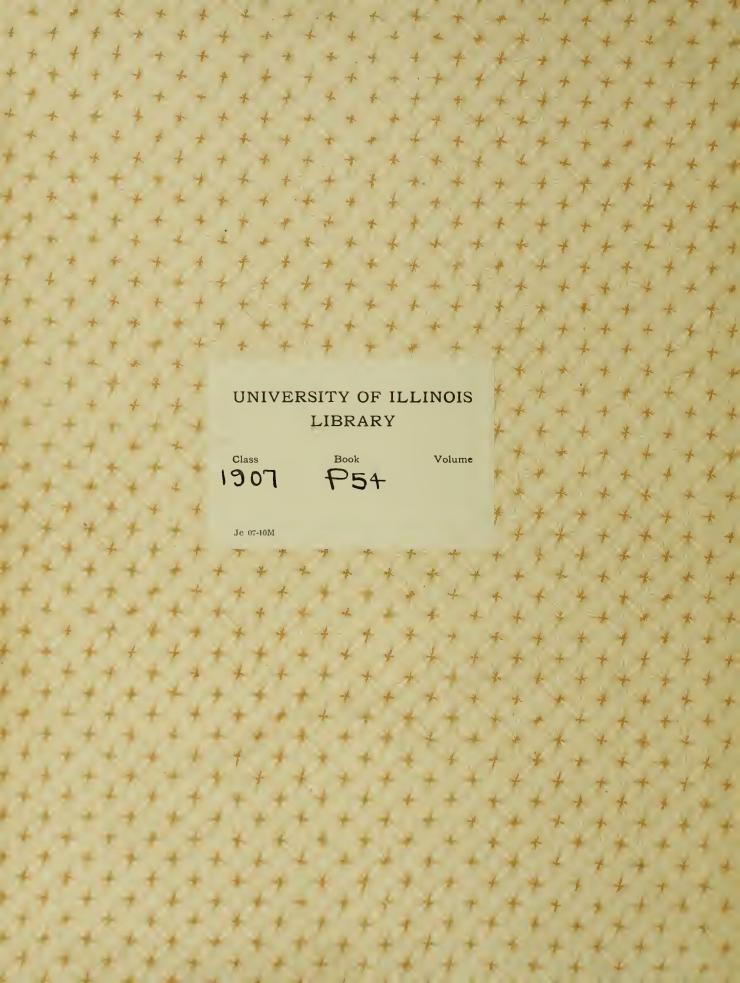
PHILLIPS

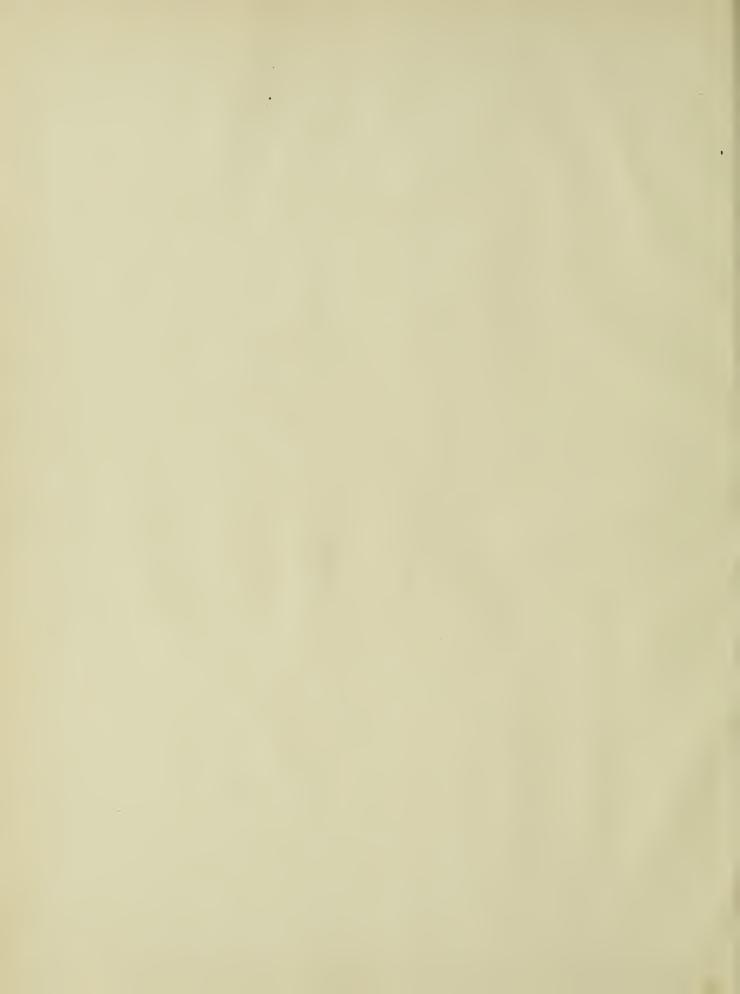
Discharge
of
Water Through Submerged
Orifices

Civil Engineering B. S. 1907









# DISCHARGE

OF

# WATER THROUGH SUBMERGED ORIFICES

BY

GUY DERRICK PHILLIPS

# THESIS

FOR

## DEGREE OF BACHELOR OF SCIENCE

IN

CIVIL ENGINEERING

COLLEGE OF ENGINEERING

UNIVERSITY OF ILLINOIS

PRESENTED JUNE, 1907

a my horse

## COLLEGE OF ENGINEERING

May 24, 1907.

This is to certify that the following thesis prepared under the direction of Professor A. N. Talbot, Head of Department of Municipal and Sanitary Engineering, by

#### GUY DERRICK PHILLIPS

entitled DISCHARGE OF WATER THROUGH SUBMERGED ORIFICES

is accepted by me as fulfilling this part of the requirements for the Degree of Bachelor of Science in Civil Engineering.

Iral. Baker

Head of Department of Civil Engineering



## INTRODUCTION.

The subject, DISCHARGE OF WATER THROUGH SUBMERGED ORIFICES, is one upon which but little experimental work has been done as compared with the free discharge of water through orifices into air. It is strange that this should be so considering the number of important uses for submerged orifices. At the present time submerged orifices are used for measuring or estimating the flow of water to and from filter beds, reservoirs, and from canals to power plants. They are often used too, but not as a measuring device, for tide-gates, and for the discharge of waste water through dams.

Previous experiments on this subject have generally been made for the purpose of determining the coefficients of discharge for effective heads of 0.5 ft. or over, but as lower heads than these are very often used there is need for data with low heads.

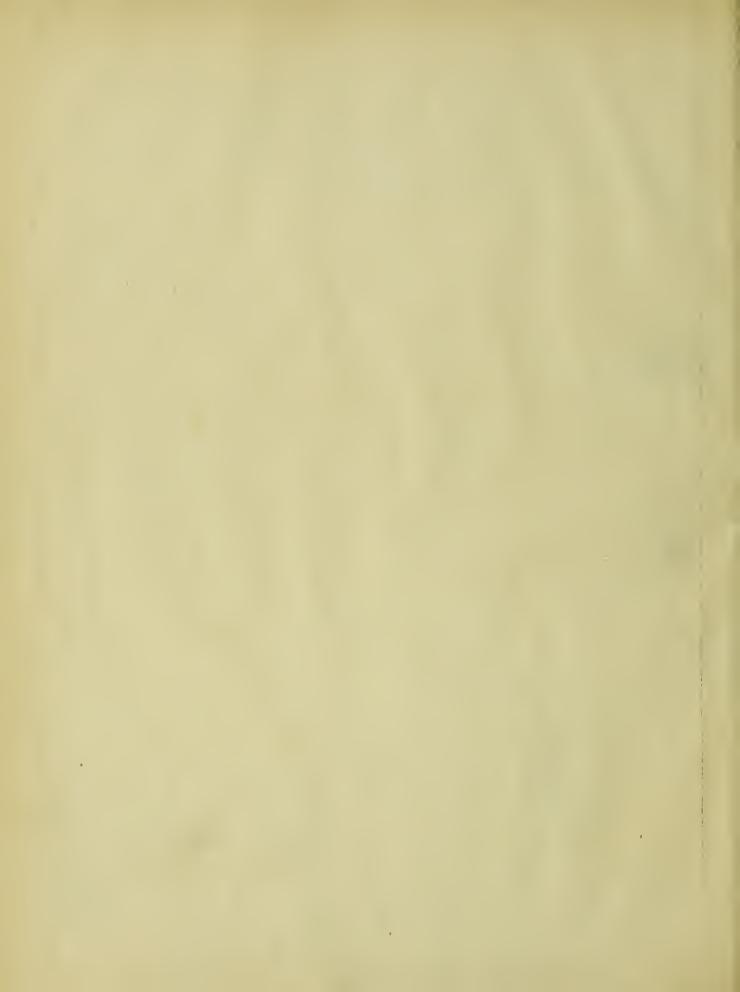
Some experimentors in this line of work state that the coefficient of discharge for a submerged orifice is the same as the coefficient of discharge for an orifice discharging freely into the air. Others say that the coefficients are from 2% to 5% less than for free discharge. To find which of these two views is correct and to determine the value of coefficients for low heads form the main objects of this thesis.

Experiments of interest along this line were first carried on by James B. Francis in 1854, and again by Hamilton Smith Jr. in 1884.



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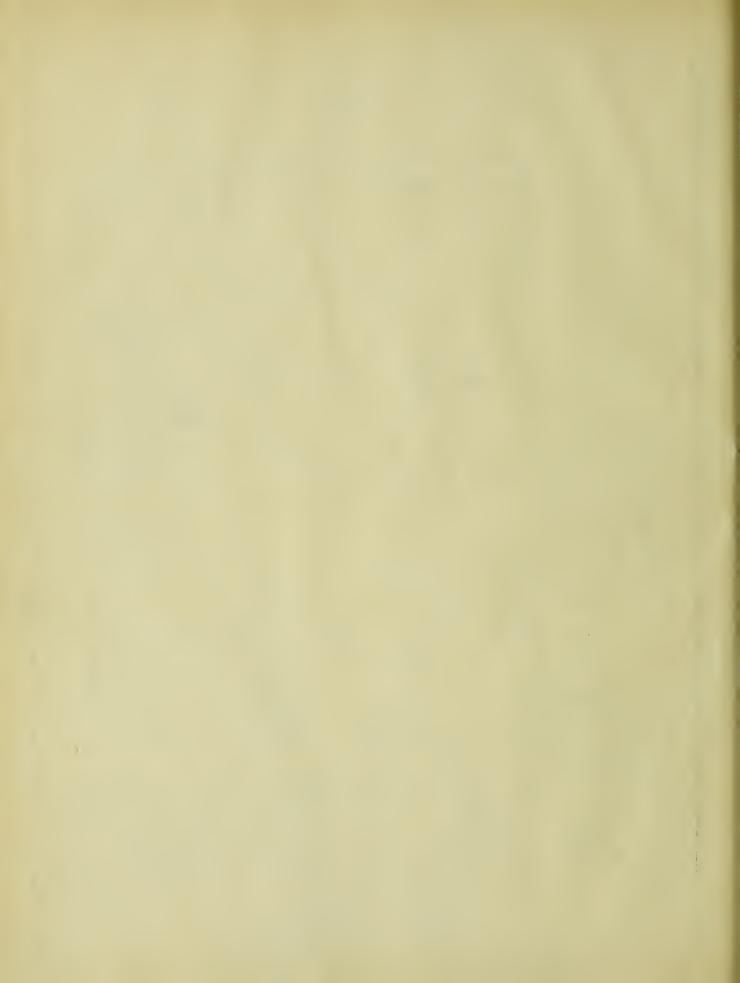
The order of presentation in this thesis will be as follows: - I. Theory; II. Methods of Experimentation; III. Sources of Error; IV. Plates and Tables; V. Discussion Of Results and Conclusions..



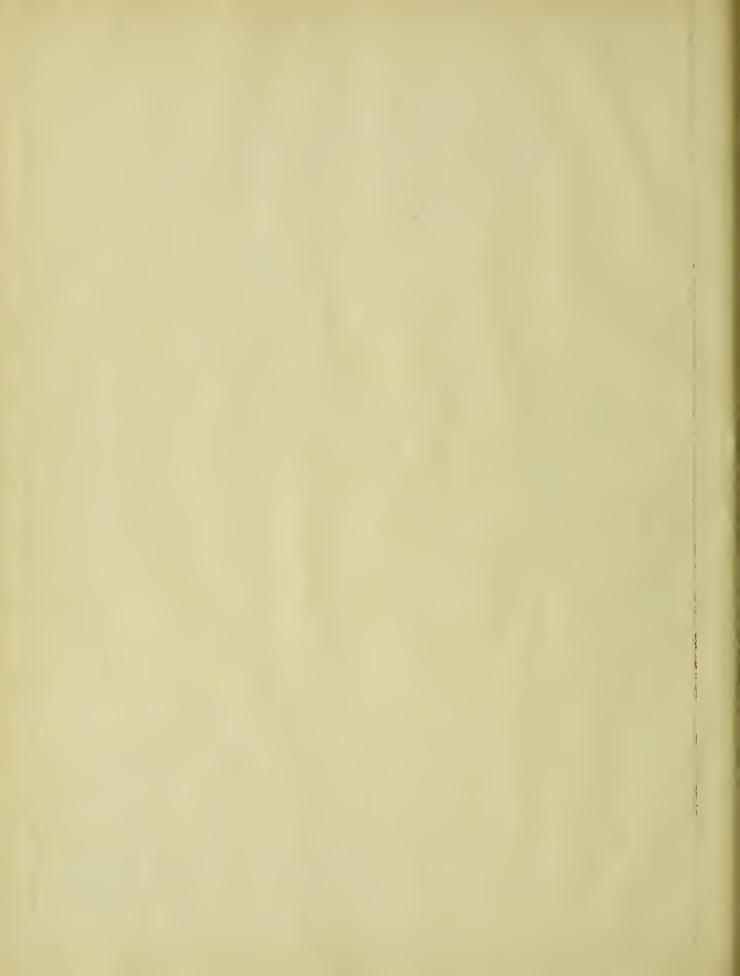
#### THEORY.

The effective head, or head which causes the flow of water through a submerged orifice, is the difference in level between the water on one side of the orifice and that on the other. This head in producing the discharge is used up in two ways, Ist. by entrance head which relates to the contraction and expansion of the stream, and 2nd. by giving velocity to the stream. The equation which shows the above relation is  $h = m \frac{V^2}{2q} + \frac{V^2}{2q}$ , or  $h = (m+1) \frac{V^2}{2q}$ , where h is the head on the orifice, or head causing the flow,  $m \frac{\sqrt{2}}{2q}$  represents the head used up in entrance expansion and losses, and  $\frac{v}{2q}$ represents the head giving velocity. In the equation V is the average velocity through the orifice in feet per second, q is the acceleration due to gravity, taken as 32.2 ft. per second, and m is the coefficient of loss due to entrance. The term  $\frac{y^2}{2q}$  is commonly termed "velocity head". The value for m is obtained from the expression  $m = \frac{1}{C^2} - 1$  (See Merriman's Hydraulics, Art. 85, 1905 Edition) where C is the coefficient of discharge and is obtained by dividing the actual discharge by the ideal discharge which is avaqh , where a is the . area of the orifice.

The value of C may be determined from the equation  $C = \frac{q}{a\sqrt{2gh}}$  where q is equal to the actual discharge in cubic feet per second. This equation may be written  $c = \frac{q}{8.02a \text{ (h)}}$ 



In this thesis the value of m which results from the experimental work, has not been calculated. All other members of the equations given have been determined as accurately as possible.

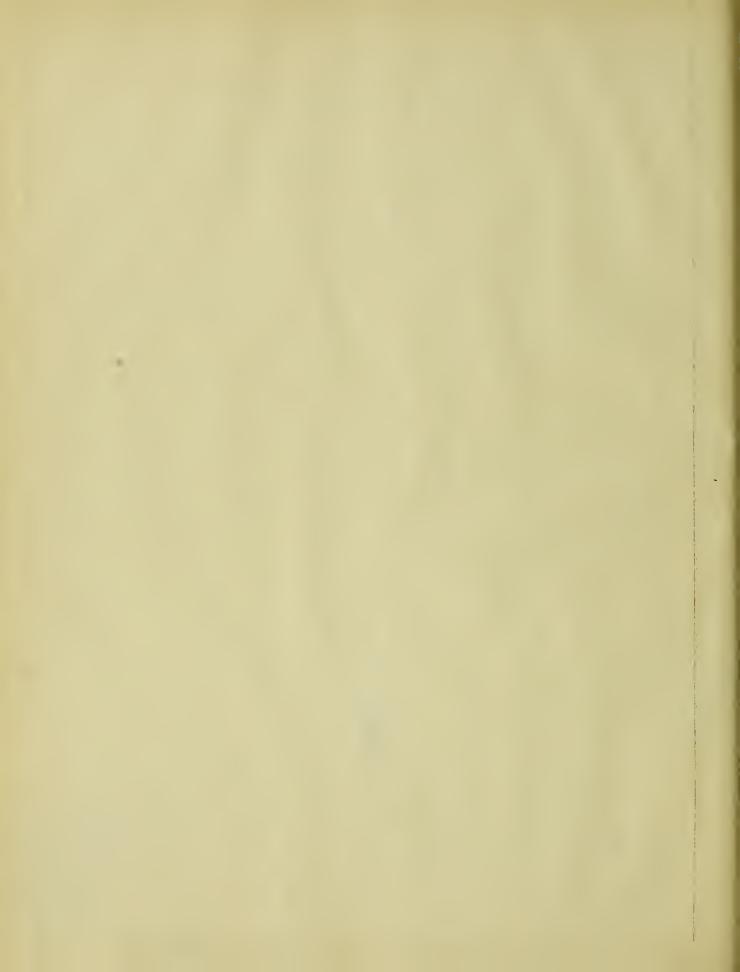


#### METHODS OF EXPERIMENTATION.

In all the experiments here-in described, the orifices used were made of cast iron plates 1-2 inch thick, with
the opening cut out of the center. The orifices tested were
of different shapes, some being circular, some square, and
still others rectangular. All plates had the orifice hole
beveled from one face to the other at an angle of 45° (See
Plate II for general form of orifices.)

These plates fitted in the lower central part of the partition of the orifice box. This partition was so constructed that it was water tight except for the orifice. Plate I gives the plan and end view of the orifice box.

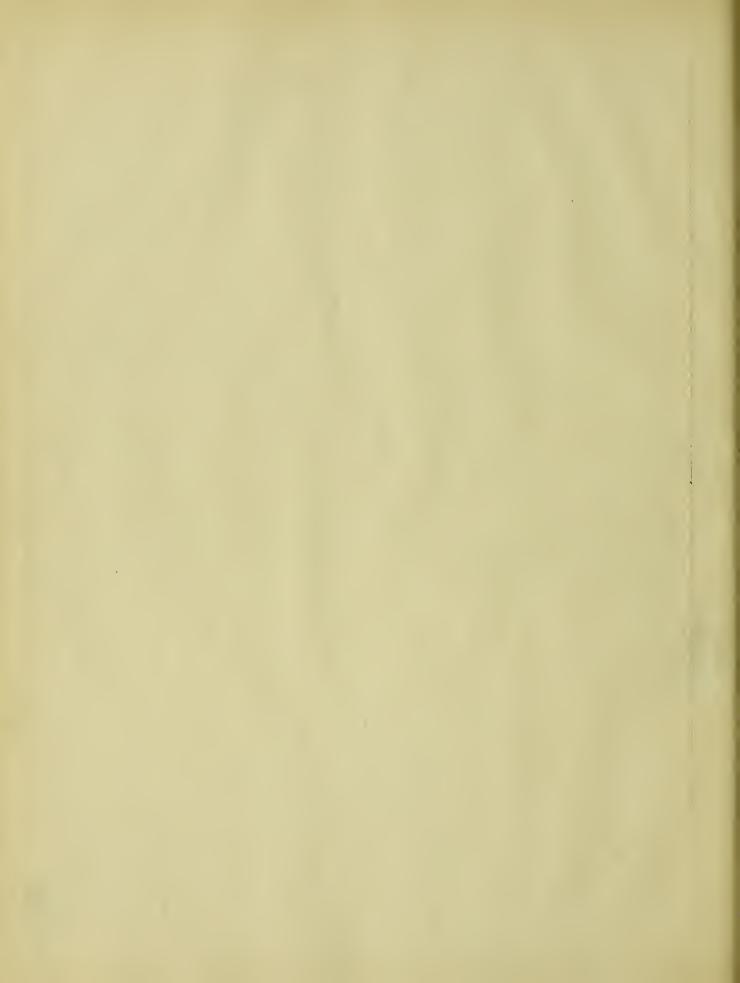
Water was admitted into the tank through a 6-inch pipe, flowed through baffle boards into compartment A, then through the orifice into compartment B, and out through two vertical openings in the end of the box. From there an 8-inch galvanized iron pipe led to the measuring pit. The vertical openings were covered by baffle-boards which kept the water at any desired height. In these baffle-boards were holes in which corks were placed or removed according to the desire to decrease or increase the discharge. In experimenting with some of the small orifices it was found necessary to nail sacks around the boards in order to obtain a very small discharge.



The difference in level in the two compartments, which is known as the discharge head, or head causing the flow, was measured by means of two vertical glass tubes, one connected with one compartment, and the other connected with the second compartment, and fastened one on each side of a scale reading to millimeters as shown in Plate I.

The water discharged, was measured in a circular concrete pit 7.995 feet in diameter and about 6 feet deep. A float and level rod graduated to hundreds of a foot were used in measuring the rise in the pit.

A set of experiments consisted of readings taken with various effective heads, most of them being under 0.5 feet. In making these experiments the water was wasted until running at a steady head, then was measured for a period rangeing from 100 to 900 seconds, and wasted again.



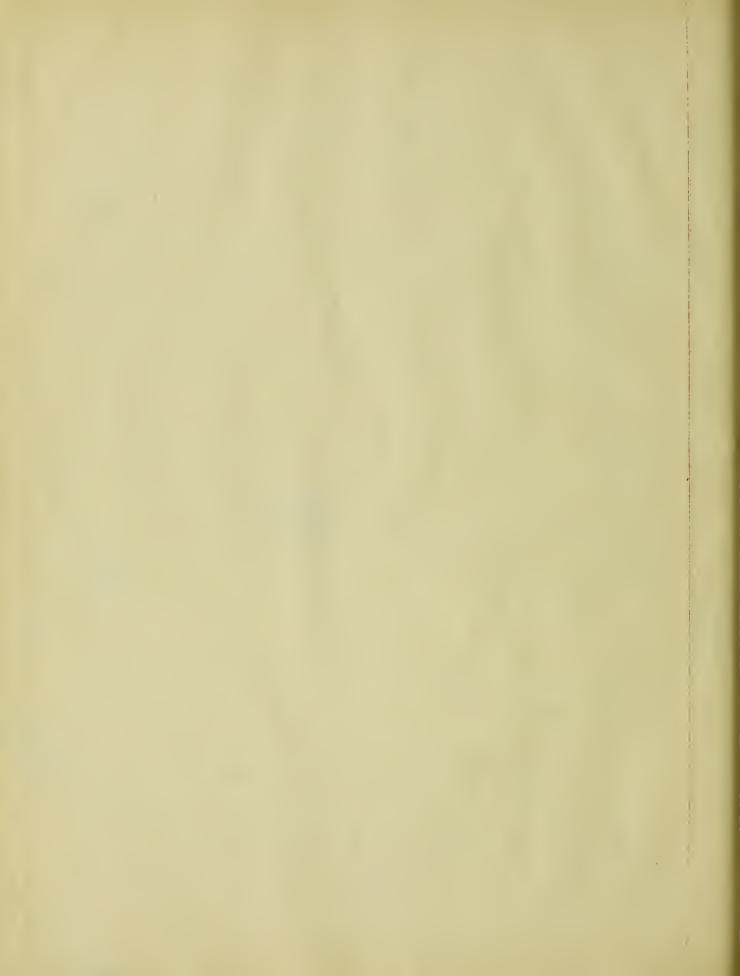
### SOURCES OF ERROR.

The probable sources of error which arose are as follows:-

The diameter assumed for the pit is that used by Mr. C. C. Wiley ('04 University of Illinois) in his experiments. It was the means of thirty readings carefully taken. The largest variation from the means of these experiments was 0.008 feet. Hence, the maximum error will not be over 0.10%.

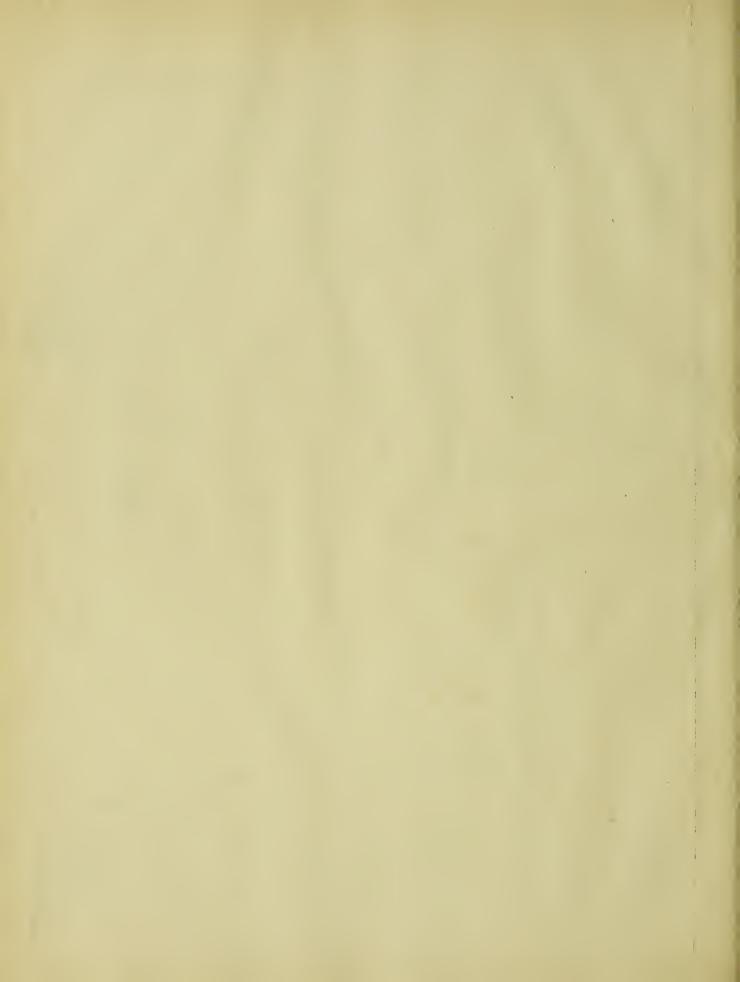
In measuring with the float and level rod the greatest variation in reading would not exceed .Ol ft. Hence the maximum error would occur where the smallest rise in the pit (0.49 ft.) was recorded. This case would give a maximum error of 2.04%. This was an exceptionally low rise the average rise being about 1.00 ft. thus reducing the error to about 1.00%.

The water in the reasuring tubes stood quite still as a rule and an effort was made to read the level to half a millimeter or .0016 ft. Therefore, with the smallest head (0.085 ft.) the maximum error would occur. This error would then be 1.88%. The average error from this source, however, would amount to a great deal less than this. For example, for a head of .225 ft. the error would be 0.71%.



watch to the nearest second. The shifting of the pipe took about half a second, consequently the maximum error would occur when the shortest time 100 seconds was used. This would give a maximum error of 0.50%.

All of these maximum errors would not occur at the same time. Besides it is the square root of h and not h itself which occurs in the results so that the greatest error under low heads probably does not exceed 4.5%. In the later tests made, where the time was greater and the rise in pit larger, the total error would probably in no case exceed 1.25%.



#### EXPLANATION OF TABLES AND PLATES.

The tables and plates given are arranged as follows:-

Table I gives the general results of all the experiments made, including the readings taken and coefficients deduced.

Table 2 gives the values of the coefficients of discharge for the various orifices experimented with under different heals as taken from the curves.

Table 3 shows the velocity of the water flowing through the various orifices, under different heads.

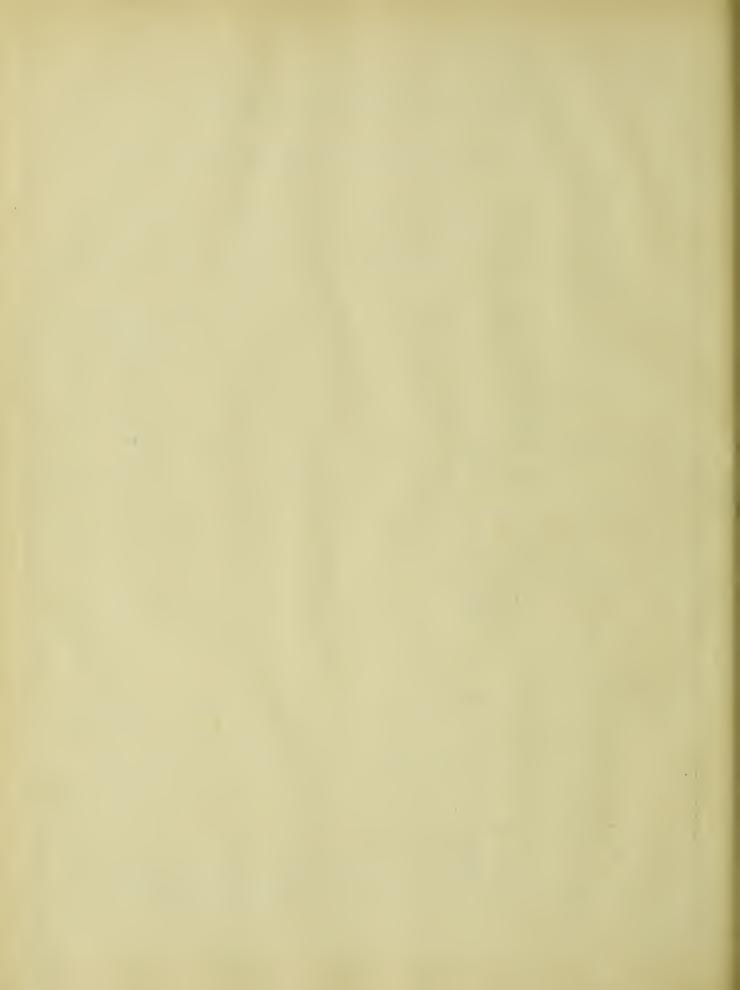
Plate I shows a cross section and end view of the orifice box used throughout the experiments.

Plate I gives the general form of orifice plate used in the experiments, with dimensions.

Plate III contains photographs of the orifice box used, the measuring pit, and the general arrangement of the apparatus.

Plate IX to IX contain curves showing the relation between the coefficient of discharge (c) and the effective head (h) for the six different orifices. They also show curves plotted from values obtained by Hamilton Smith Jr. in 1884 for free discharge.

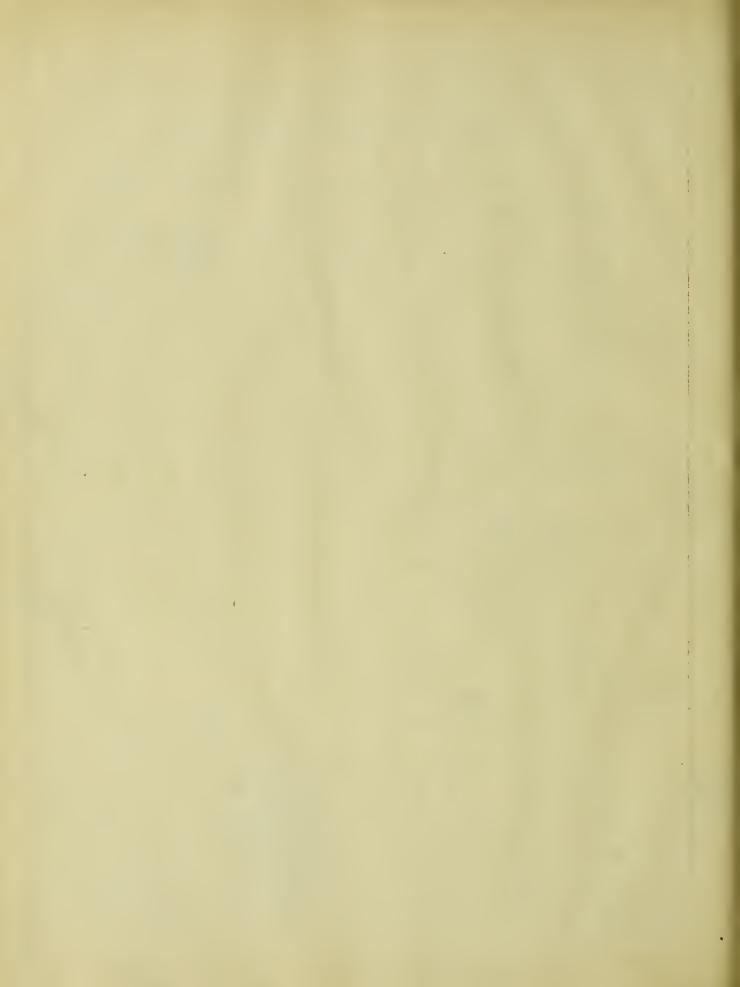
Plate X shows a comparison of the different coefficients of discharge for the different shaped orifices.



#### DISCUSSION OF RESULTS AND CONCLUSSIONS.

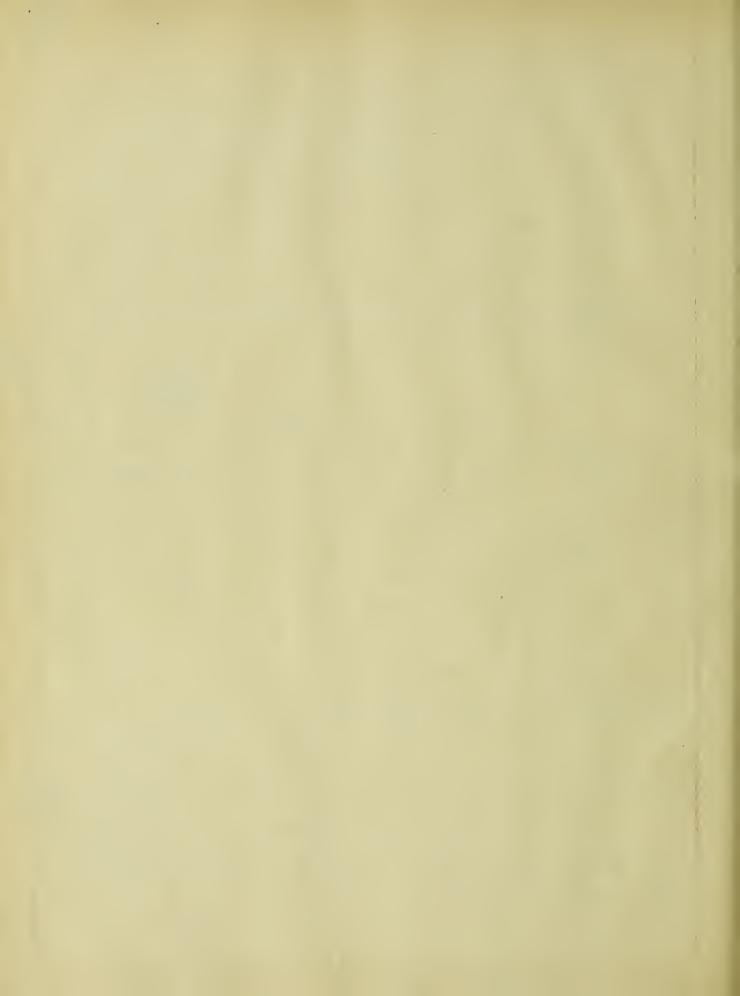
From the data experimentally determined, the following conclustions may be drawn:-

- (I) Of the two series of experiments performed on some of the orifices, the results of the second set are to be relied upon to a far greater extent than those of the first. This is due to the fact that the first series were performed with only a small rise of water in the reasuring pit, while in the other set, a rise from two to three times as great was used. Consequently there was not such a probability of error and wide range of values for coefficients.
- (2) The separate orifice curves contained in Plates IX to IX represent the most probable values of the coefficients of discharge for the submerged orifice.
- (3) Without any exception the diagrams appear to be straight lines for heads of 0.2 ft. or over. For heads between 0.1 ft. and 0.2 ft. the rise in coefficients is very small, the extreme case being .004.
- (4) The curves plotted on Plate X show that, the larger the opening in the orifice the smaller the coefficient of discharge. Thus there is a range of 013 between a 6-inch and a 2-inch circular orifice. For the square ones the same is true, there being a difference of .009 between a 2-inch and a 4-inch. From the one rectangular orifice experimented with it can be plainly seen that this orifice gives the



largest coefficients of discharge. This is shown by the fact that the principal contraction is on two sides of the orifice. The values obtained from this orifice were on an average of 1.62% higher than for orifices with a much smaller opening. Scarcely any difference is shown between the coefficients of a circular orifice and a square shaped orifice. This seems rather odd as we naturally expect a larger coefficient for the square than for the circular since there is less contraction on the former than on the latter.

(5) Coefficients of discharge for submerged orifices are undoubtedly larger than those for free discharge. A comparison of the curves on Plates IX to IX readily show this. The coefficients of discharge as determined from these experiments are from 1.67% to 0.55% larger than for free discharge through orifices of the same shape and size as determined by Hamilton Smith Jr. in 1834. In only one case are the values given here smaller than those for free discharge, that being for the 4-inch square orifice where the values for submergence are 0.49% less. This can only be accounted for by a constant error in determining the values for the 4-inch square, but even this seems hardly probable, as the results determined were more nearly constant than for any other orifice. A difference of 1.0% is probably a safe average for values of submerged and free discharging orifices.

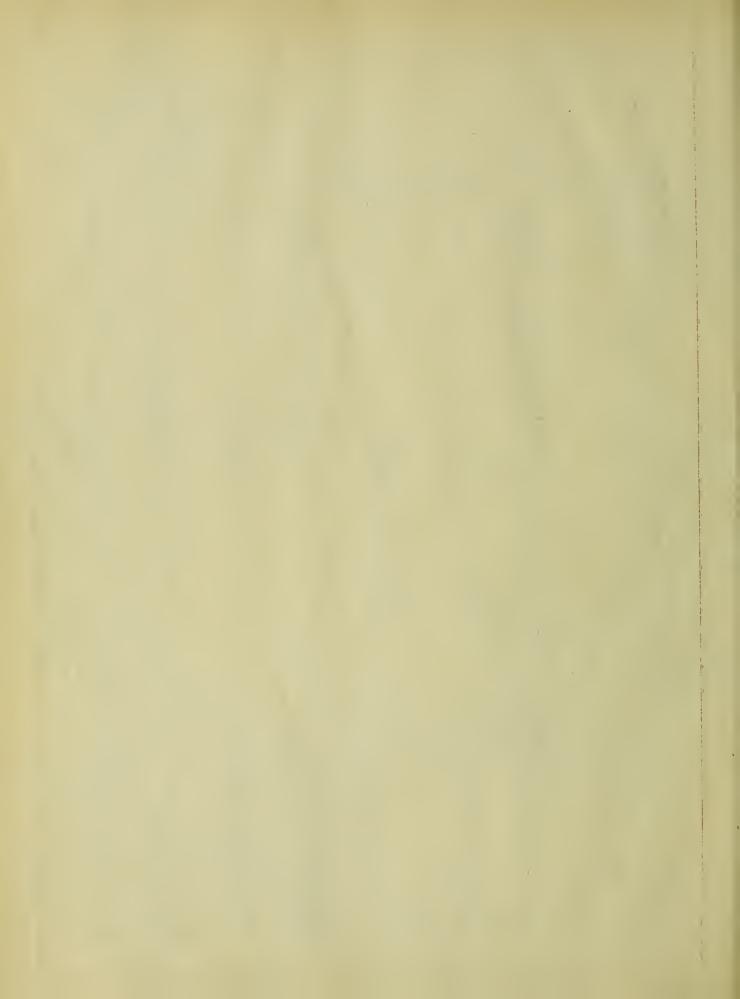


Hamilton Smith Jr. has probably done the greatest amount of experimenting to date in this line, but in no case has he determined values for effective heads under 0.5 ft.

Work of this kind is very interesting and there is undoubtedly a great deal of work which may yet be done along this line.



1	2	3	4	5	6	7	8	9
Ref	Kind of Orifice	Effect- ive Head in Feet "h"	Time in Seconds	Rise in Pit Feet	Actual Dis- charge "q" Cu. Ft. per Sec	Q-aV2gh Cu. Ft. per Sec	Coef. of Dis- charge "c"	Average Actual Vel. Feet per Sec
1234567890112345678901123145617890222245678001233456789044234456	4-in. Cir- Cir- Cilar	0.156 0.152 0.150 0.144 0.153 0.172 0.274 0.375 0.384 0.375 0.384 0.509 0.514 0.626 0.770 0.144 1.220 1.220 1.320 1.610 0.274 0.	147 205 210 170 140 185 170 135 140 270 135 140 220 125 130 120 125 125 125 120 125 125 120 125 120 125 120 120 120 120 120 120 120 120 120 120	0.49 0.68 0.71 0.46 0.75 0.46 0.75 0.88 1.74 1.35 0.95 1.35 0.95 1.40 1.54 1.54 1.54 1.54 1.55 1.56 1.56 1.56 1.56 1.56 1.56 1.56	0.168 0.168 0.170 0.163 0.166 0.178 0.195 0.225 0.260 0.265 0.303 0.305 0.302 0.307 0.340 0.425 0.470 0.472 0.481 0.224 0.220 0.415 0.224 0.220 0.193 0.194 0.195 0.195 0.195 0.210 0.205 0.200 0.463	0.275 0.275 0.275 0.275 0.275 0.275 0.275 0.275 0.275 0.299 0.365 0.439 0.434 0.501 0.5501 0.5501 0.775 0.775 0.775 0.775 0.775 0.775 0.3671 0.499 0.321 0.499 0.321 0.321 0.236 0.3361 0.321 0.236 0.3369 0.	0.609 0.615 0.618 0.611 0.608 0.611 0.602 0.606 0.611 0.609 0.609 0.612 0.609 0.612 0.609 0.613 0.609 0.618 0.602 0.618 0.602 0.618 0.602 0.618 0.603 0.618 0.603 0.618 0.601 0.603 0.618 0.601 0.603 0.601 0.603 0.601 0.603 0.601 0.603 0.603	1.996715/40\800459084\8005/9\715\80\8005\9\7\5\8\80\80\80\80\80\80\80\80\80\80\80\80\8



1	2	3	4	5	6	7	8	9
47 48 49 50 51 52 53 54	4-in. Cir- cular.	1.221 0.983 0.925 1.120 1.065 (0.496 0.508 0.510	155 200 205 220 200 270 300 260	1.49 1.70 1.69 2.00 1.77 1.63 1.81 1.58	0.480 0.425 0.411 0.454 0.442 0.300 0.301 0.305	0.789 0.699 0.677 0.745 0.726 0.493 0.496 0.500	0.610 0.609 0.610 0.610 0.610 0.608 0.608	5.51 4.89 4.74 5.21 5.09 3.45 3.46 3.51
55 56 57 58 59 60 62 63 64 65 66 67 68 69 71 72	6-in. Cir- cular.	0.120 0.118 0.120 0.120 0.146 0.145 0.275 0.275 0.276 0.258 0.444 0.447 0.436 0.441 0.711 0.711	340 250 300 240 240 260 265 180 205 170 230 270 260 240 210 220 205 220	2.24 1.61 1.95 1.57 1.73 1.85 1.92 1.77 2.01 1.68 2.19 3.38 3.25 2.99 2.61 3.48 3.24 3.49	0.328 0.324 0.326 0.328 0.360 0.356 0.363 0.494 0.496 0.475 0.624 0.625 0.621 0.622 0.790 0.790 0.792	0.541 0.539 0.542 0.542 0.599 0.594 0.600 0.811 0.811 0.796 1.043 1.043 1.043 1.038 1.041 1.320 1.320 1.322	0.601 0.600 0.600 0.600 0.599 0.599 0.599 0.599 0.598 0.598 0.598 0.598	1.64 1.66 1.65 1.64 1.83 1.82 1.84 2.51 2.52 2.42 3.18 3.18 3.15 3.16 4.02 4.02 4.02
73 74 75 76 77 78 79 81 82 83 84 85 86 88 99 91 92 93 95	2-in. Cir- cular.	0.338 0.343 0.345 0.354 0.588 0.580 0.594 0.178 0.178 0.181 0.183 0.127 0.124 0.124 0.760 0.745 0.720 0.713 1.049 1.082	6.7:6	0.67 0.59 0.75 0.88 0.69 0.68 0.99 0.65 0.52 0.62 0.62 0.62 0.72 0.89 0.62 0.99 0.68 0.68	0.062 0.063 0.063 0.064 0.082 0.082 0.083 0.045 0.045 0.045 0.045 0.038 0.038 0.038 0.093 0.090 0.090 0.110 0.112 0.111	0.101 0.102 0.103 0.104 0.133 0.135 0.073 0.073 0.074 0.075 0.061 0.062 0.062 0.151 0.150 0.147 0.147 0.179 0.181 0.181	0.612 0.605 0.614 0.617 0.618 0.615 0.615 0.615 0.611 0.620 0.614 0.612 0.612 0.612 0.613 0.615 0.613	2.85 2.85 2.90 2.95 3.80 3.73 3.82 2.07 2.07 2.07 2.12 1.70 1.75 1.75 4.28 4.14 4.14 5.17 5.11



1	2	3	4	5	6	7	8	9
96 97 98 99 100	Cir- cular	1.081 1.080 1.460 1.424 1.426 1.422	310 330 310 360 305 420	0.69 0.73 0.79 0.92 0.78 1.07	0.111 0.111 0.128 0.128 0.128 0.128	0.182 0.182 0.210 0.208 0.208 0.207	0.611 0.611 0.610 0.614 0.613 0.613	5.11 5.11 5.89 5.89 5.89 5.89
102 103 104 105 106 107 108 109 110 111 112 113 114 115 117 118 120 121 123 125 126 127 128 120 131 132 133 133	square 6	1.687 1.659 1.661 1.683 (1.038 1.007 0.990 (0.679 0.682 0.684 0.697 0.709 0.118 0.114 0.113 0.112 0.118 0.164 0.165 0.16	290 420 285 330 360 360 420 420 360 360 360 540 480 900 660 720 660 660 765 480 540 480 540 480 540 480 540 680 680 680 680 680 680 680 68	1.02 1.47 1.00 1.15 1.07 0.99 0.97 1.14 0.95 0.79 0.80 0.79 1.37 1.10 0.32 0.66 0.66 0.65 0.65 0.65 0.65 0.65 0.65	0.176 0.175 0.175 0.175 0.138 0.138 0.136 0.136 0.137 0.110 0.111 0.110 0.113 0.114 0.045 0.045 0.045 0.045 0.045 0.045 0.055 0.055 0.055 0.055 0.055 0.078 0.079 0.079 0.078 0.096 0.096 0.098 0.097	0.289 0.287 0.287 0.286 0.227 0.229 0.224 0.221 0.162 0.183 0.184 0.185 0.186 0.187 0.073 0.075 0.073 0.074 0.090 0.090 0.090 0.128 0.130 0.128 0.158 0.160 0.161	0.610 0.610 0.610 0.608 0.609 0.611 0.600 0.600 0.600 0.610 0.613 0.611 0.613 0.610 0.608 0.610 0.609 0.610 0.609 0.610 0.609 0.610 0.609 0.610 0.609 0.610 0.609 0.610 0.609 0.610 0.609	6.33 6.30 6.30 6.30 6.37 4.97 4.88 4.97 3.95 4.88 4.10 1.62 1.62 1.62 1.98
134 135 136 137 138 139 140 141 143 144 145 146 147		0.089 0.086 0.086 0.085 0.164 0.163 0.163 0.213 0.213 0.219 0.215 (0.174 0.166 0.166	480 540 495 520 170 120 190 160 100 120 120 120 120	1.53 1.70 1.54 1.62 0.73 0.52 0.82 0.79 0.49 0.60 0.60 0.67 0.52 0.61	0.160 0.158 0.157 0.157 0.215 0.216 0.216 0.247 0.246 0.250 0.250 0.224 0.218 0.219	0.264 0.260 0.260 0.261 0.356 0.356 0.409 0.415 0.415 0.412 0.369 0.360 0.361	0.604 0.605 0.603 0.601 0.600 0.604 0.603 0.605 0.605 0.603	1.44 1.43 1.43 1.94 1.95 1.95 2.24 2.22 2.25 2.01 1.96 1.97



1 2	3	4	5	6	7	8	9
148 4-in. 149 square 150 151 152 153 154 155 156 157 158 159 160 161 162 163 164 165 166 167 168 169 170	0.164 /0.350 0.355 0.315 0.627 0.622 0.626 0.603 0.573 0.607 0.609 /0.109 (0.109 0.153 /0.152 0.146 0.149 0.335 0.338 7.068 (1.068 (1.077 1.096	125 155 175 155 195 140 155 170 300 240 270 185 480 480 425 420 270 295 280 260 230	0.54 0.98 1.11 0.93 1.16 1.30 1.43 2.50 1.94 2.25 1.55 1.68 1.68 1.77 1.71 1.73 1.67 1.82 3.10 2.88 3.13	0.217 0.315 0.316 0.300 0.299 0.423 0.420 0.420 0.416 0.416 0.419 0.176 0.208 0.208 0.209 0.205 0.310 0.310 0.553 0.555 0.561	0.359 0.525 0.528 0.497 0.498 0.705 0.699 0.702 0.691 0.673 0.690 0.695 0.294 0.294 0.347 0.346 0.341 0.517 0.920 0.930	0.602 0.600 0.601 0.602 0.600 0.599 0.598 0.601 0.601 0.601 0.600 0.600 0.600 0.600 0.600 0.601 0.600 0.600 0.600 0.600 0.600	1.96 2.85 2.85 2.70 2.70 3.80 3.75 3.76 3.55 3.76 3.71 1.59 1.59 1.88 1.85 1.86 2.80 5.00 5.01 5.08
171 6-in.x 172 1-in. 173 Rect. 174 175 176 177 178 179 180 181 182 183 184 185 186 187 188 189 190 191 192 193 194 195 196 197 198 199 190	0.110 0.110 0.108 0.108 0.157 0.156	635 600 780 705 505 410 660 540 680 595 500 480 620 420 630 480 395 540 315 555 300 345 480 240 250 330	0.88 0.82 1.07 0.97 0.69 0.67 1.09 0.89 1.11 0.98 1.05 0.99 1.25 1.30 1.54 1.15 0.95 1.30 1.14 1.22 1.43 1.99 1.12 1.25 1.35 1.75	0.069 0.069 0.069 0.069 0.069 0.083 0.083 0.083 0.105 0.104 0.105 0.123 0.122 0.120 0.120 0.120 0.120 0.164 0.164 0.164 0.164 0.164 0.164 0.206 0.207 0.203 0.270 0.270	0.110 0.111 0.110 0.110 0.131 0.132 0.131 0.139 0.169 0.169 0.169 0.197 0.196 0.193 0.193 0.193 0.193 0.264 0.265 0.260 0.261 0.330 0.332 0.335 0.423 0.432	0.627 0.621 0.620 0.629 0.632 0.622 0.632 0.631 0.627 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623 0.623	1.66 1.66 1.66 1.66 1.99 1.99 1.99 1.99

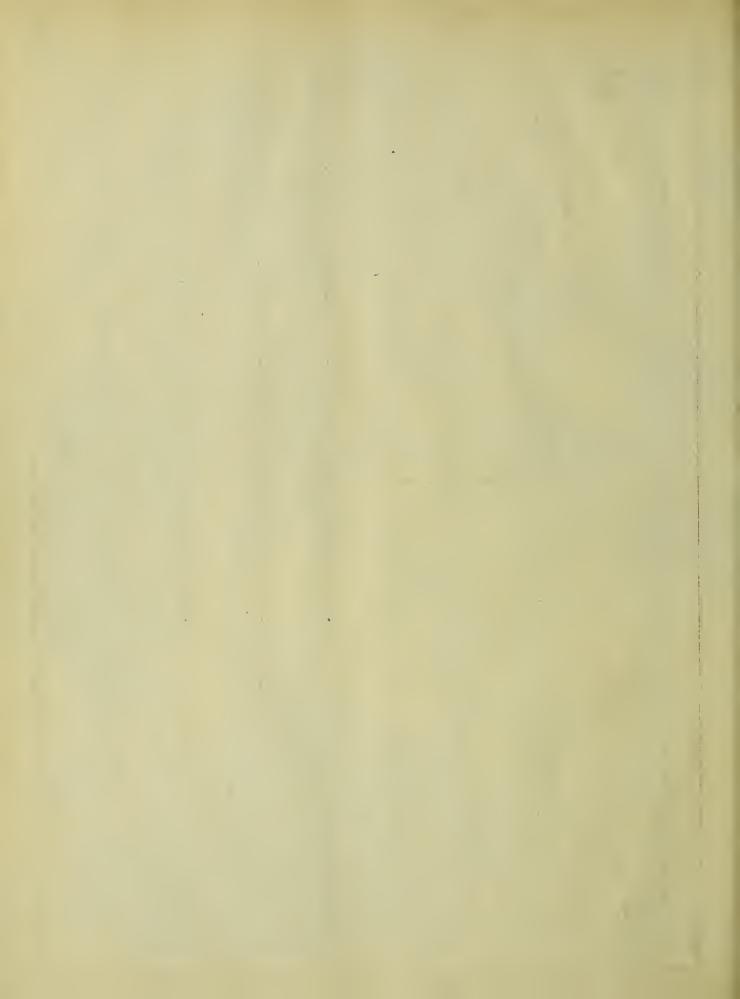


TABLE 2

## COEFFICIENTS OF DISCHARGE DETERMINED

FOR

SUBMERGED ORIFICES

FROM

CURVES.

Effect-	King of Origice.						
Head h in Feet	2-in. Circul <b>a</b> r	4-in.	6-ir. Circular	2-in. Square	4-in. Square	6in Xlin Rect.	
0.10 0.15 0.20 0.30 0.40 0.50 0.75 1.00 1.50 2.00	0.614 0.613 0.613 0.613 0.613 0.613 0.613 0.613	0.609 0.609 0.609 0.609 0.609 0.609 0.609	0.601 0.600 0.599 0.599 0.599 0.599	0.611 0.610 0.610 0.610 0.610 0.610 0.610 0.610	0.603 0.601 0.601 0.601 0.601 0.601	0.625 0.624 0.623 0.622 0.622 0.622 0.622 0.622 0.622 0.622	

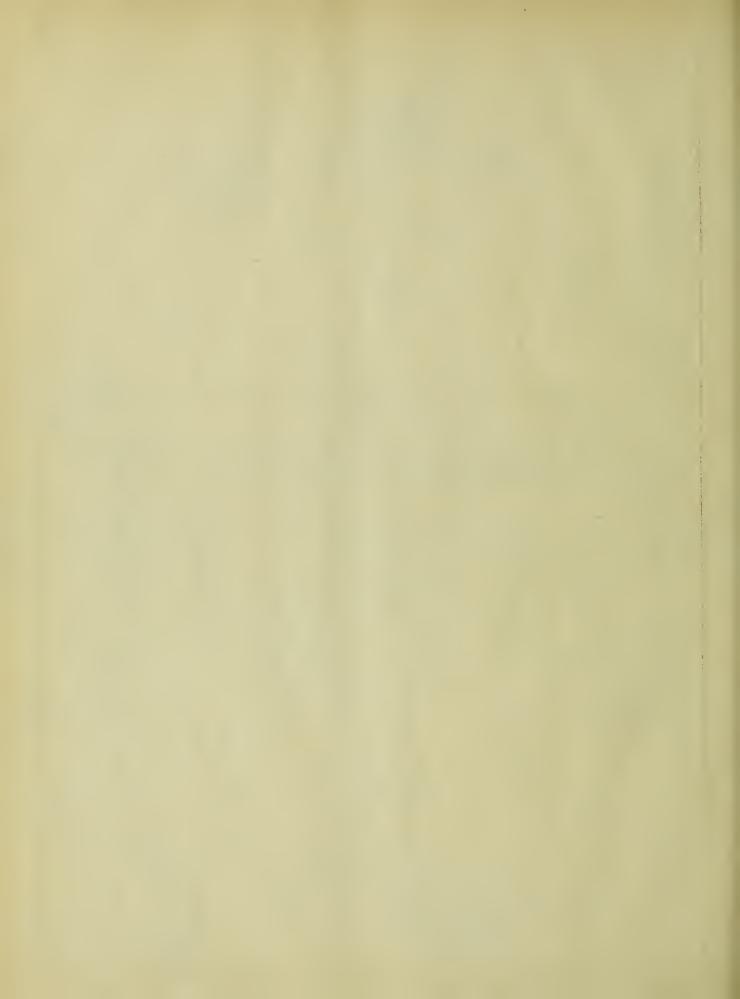


TABLE 3

### AVERAGE VELOCITY OF WATER

## THROUGH SUBMERGED ORIFICES

IM

FHET PER SECOND.

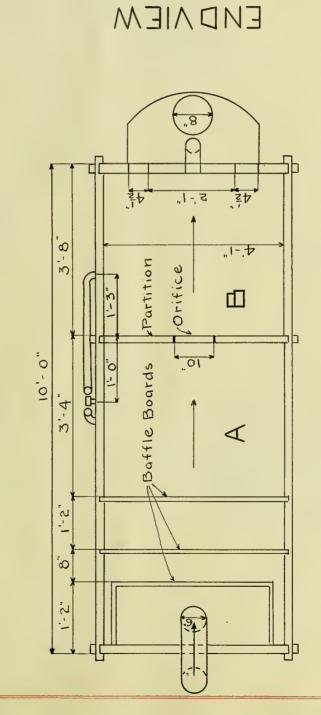
Effect-	Kind Of Orifice.							
Head h in Feet.	2-in. Circular	4-in. Circular	6-in. Circular	2-in. Square	4-in. Square	6in x lin Rect.		
0.10 0.15 0.20 0.30 0.40 0.50 0.75 1.00	1.61 1.87 2.15 2.92 3.01 3.40 4.25 5.01 5.92	1.60 1.90 2.20 2.70 3.02 3.48 4.21 4.90 6.21	1.53 1.85 2.10 2.68 2.96 3.46 4.06	1.58 1.80 2.19 2.66 2.99 3.46 4.08 4.92 6.18	1.56 1.82 2.18 2.61 2.97 3.50 4.17 4.93	1.60 1.92 2.25 2.72 3.08 3.42 4.29 4.29 6.29		



PLAN AND END VIEW

OF

ORIFICE BOX



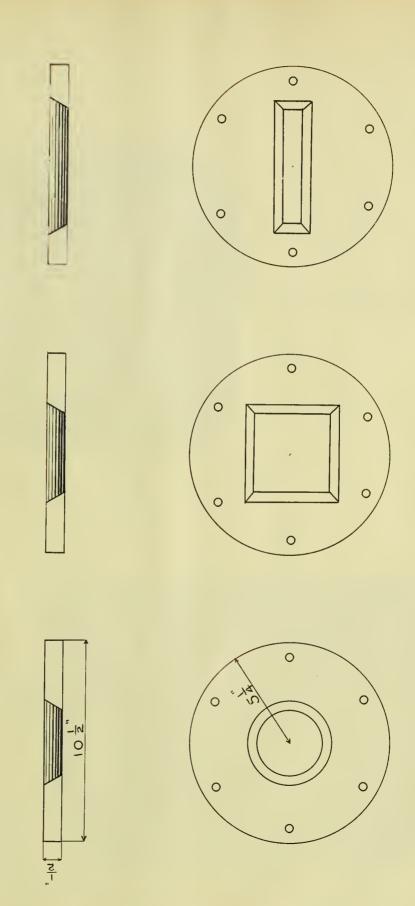
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100L

PLAN



# TYPICAL ORIFICE PLATES





# PLATE III



DRIFICE BOX

MEASURING PIT





h. Effective Head in Feet.



h. Effective Head In Feet



h - Effective Head in Feet

1090 to 1000 t

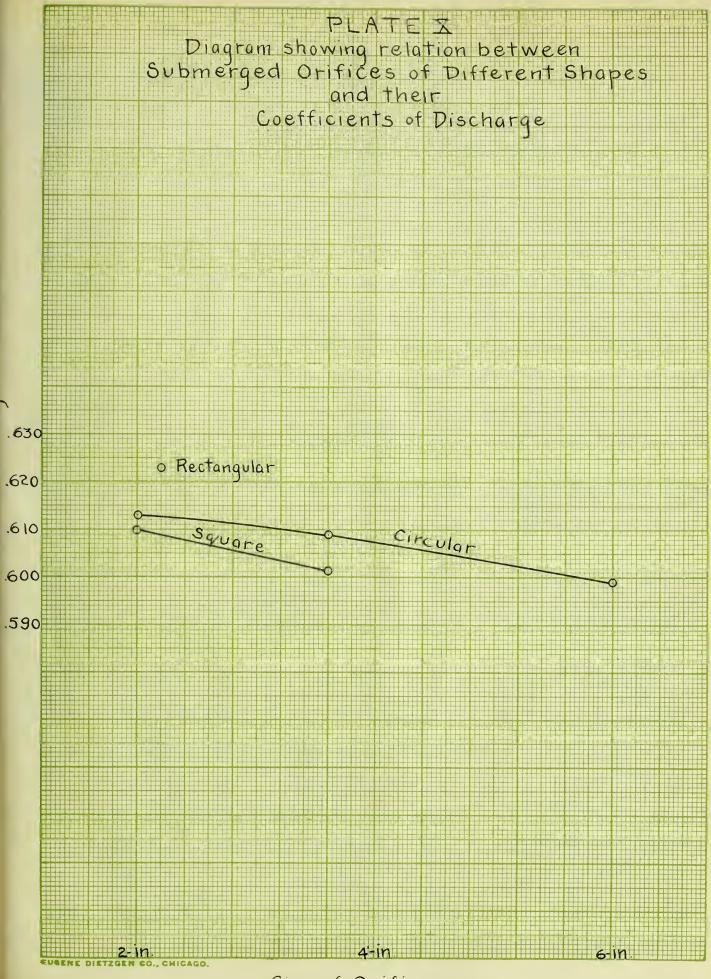
h. Effective Head in Feet



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Size of Orifice



